

To predict transitional and fully developed turbulent flow in a backward facing step geometry

This was original a workshop at the COBEE 2015 conference in China

Peter V. Nielsen and Yuguo Li

Background

It is known from experiments and simulations that low Reynolds' number effects may take place in room air flow. We know that this type of flow is difficult, to predict in details by CFD due to limitations of available turbulence models in connections with RANS equations, limitations of computer capacity and limitations in other types of methods as e.g. the use of LES. Errors due to choice of numerical methods, choice of the right physical model of the engineering problem you solve, choice of relevant boundary conditions and errors due to user's experience are also a part of relevant problems in doing CFD predictions.

Significant development and improvement has taken place in the CFD community in the last 30 years and, at least, some of the above mentioned problems have been addressed. It is therefore interesting to see how far we are today collectively with the relevant software and hardware.

Invitation

We invite you to participate in a workshop which will be finalized at the COBEE conference in July 2015.

The purpose of this unique workshop is to focus on errors existing in CFD simulations, especially in connection with low turbulent flow, and discuss what we can do, using a simple method.

We present a simple CFD problem (with no benchmark or experimental data for comparison) for all participants of the workshop to simulate using well-known and widely used commercial CFD software. We ask you to send your CFD results to us, and we shall consolidate all the results, and present in the workshop.

Consider this problem was a request from your client – your client is interested to have an accurate prediction of the penetration length for the whole Reynolds number range from zero to 10,000.

All participants who have submitted the simulations are invited to join, and we will discuss together on the following topics

1. How large are the differences in CFD results? How significant are the differences? Why are there differences? What can we do to minimize potential CFD errors?
2. How are the different schemes able to handle the low turbulent flow in the selected case? How can we find/define the limits for use of different turbulence models?
3. What are the challenges in applying CFD to a problem? How to build confidence in CFD simulations?

The CFD problem

We propose a simple CFD problem that is easy for all to simulate even on your PC. It is incompressible and two-dimensional in the laminar regime and perhaps in the fully turbulent regime, but not necessarily in the transition regime. It may be considered as a simple building ventilation problem in the turbulent regime, and it is described as The Backward-Facing Step or Sudden Expansion Flow in the fluid dynamics community. The flow is isothermal.

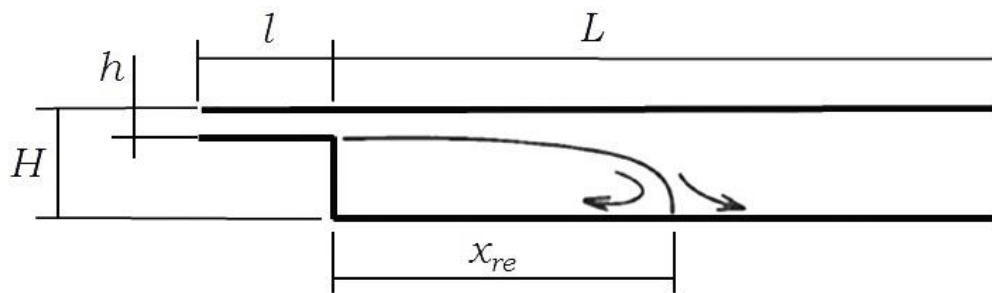


Figure 1. The geometry to use in the test case.

Figure 1 show the geometry of our proposed case. The flow is typical for isothermal room air flow in deep rooms. H , h and l are room height, supply slot height and length of supply opening.

L is the length of the model/room (note that this length should be sufficient otherwise, it may affect your prediction), and x_{re} is the length from the end wall to the location where the reattaches flow is separated in a flow back to entrainment into the wall jet and a forward flow towards the exit (i.e. reattachment point). The length x_{re} is referred to as the penetration length of the supply jet.

The following dimensions should be used:

$$h/H = 1/5$$

$$l/h = 4$$

L should have a sufficient length without influencing the obtained penetration length x_{re}/H .

x_{re} is the distance to the first reattachment in the flow (there can be more in the case of laminar flow).

The flow might be transient and three-dimensional in a certain range of Reynolds Numbers (we can at least not exclude the possibility). We will therefore also define the test case as a 3D geometry with:

$$W = 2H$$

We consider the velocity and the penetration depth in the 3D case in the vertical median plane at $y = 0.5W$.

The inlet flow is a Top Hat profile with constant velocity u_o everywhere in the profile.

The Reynolds number is:

$$Re = (h \cdot u_o) / \nu$$

Where ν is kinematic viscosity.

Requirements at the COBEE 2015 conference

You are invited to participate in a workshop where you predict the flow in the geometry from very small Reynolds numbers with laminar flow to high Reynolds numbers with fully developed turbulent flow. The range should be from $Re = 1$ to $Re = 10,000$. It is especially interesting to see if it is possible to handle the low Reynolds number regime or at least a part of it.

We ask you to select a CFD code (commercial code or your own development) and we ask you to select an appropriate turbulence model. Alternative you could also use LES. You are free to select the boundary conditions.

You are reminded to take a special care for the Low Reynolds number region. If your code or software tells you that your chosen turbulence model may not work for a particular region, please report it in your results. Do also tell us if your code gives any other warning.

You may record the effective dynamic viscosity at the recirculation centre, and plot the number of iterations as a function of the Reynolds number. These will be useful for interpretation of our results.

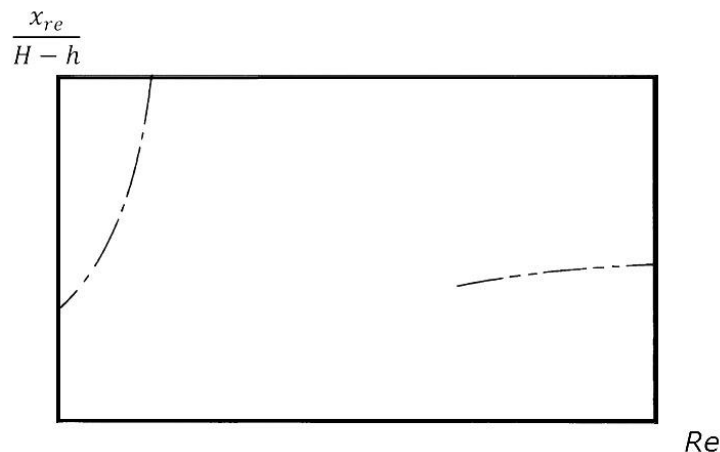


Figure 2. An illustrative graph for penetration length from $Re = 1$ to $10,000$, as predicted by CFD. Note that this is just an example, hence no scales are given.

It is shown in [Figure 2](#) that we may not obtain reliable prediction for low (not very low) Reynolds numbers (not fully developed turbulence region). You may find out what you can do for this low Reynolds number region. Do not connect results predicted by two different turbulence models in the final Excel scheme, or connect laminar predictions with predictions made by a turbulence model (which is also avoided in figure 2 in this instruction).

A benchmark test for room air distribution: The backward facing step flow

P V Nielsen, C Zhang, C T Kjær, D Leiria, H Nørholm, T Ramstad, A Rovithakis and R L Jensen

Aalborg University, Thomas Manns Vej 23, DK-9220 Aalborg Ø, Denmark

pvn@civil.aau.dk

Abstract. This paper concerns the use of Computational Fluid Dynamics (CFD) for the prediction of room air movement and provide a guide on selecting of the proper turbulence model. The benchmark which developed here for the first time is a backward-facing step flow problem. The measurements is performed in a small-scale model and the velocity filed is measured by Particle Image Velocimetry (PIV). The measurements focus on transitional flow and fully developed turbulent flow at isothermal condition. The PIV measurements and different CFD predictions are compared. The CFD predictions are generally slightly diverse, and this is, among other things, the result of using different turbulence models as well as using different software codes, grid distribution and boundary values etc. The $k-\varepsilon$ family of turbulence models is an option for fully developed flow, and the $k-\omega$ family does work for transitional low turbulent flow in this backward-facing step flow.

1. Introduction

The indoor environment community has adopted computational fluid dynamics (CFD) as a useful tool for the prediction of air movement in ventilated spaces. Researchers have used the method for many years as a research tool, see e.g. Nielsen [1] and [2]. Now, it is used routinely in civil engineering when designing a large or complicated air distribution system, Nielsen [3].

The airflow is described mathematically by a set of coupled differential equations, known as the Navier-Stokes equations. These equations are reformulated into a high number of ordinary equations and solved by a numerical method. It is necessary to add additional (partly empirical) equations for the description of the turbulence in the flow, and different turbulence models are introduced for different types of flow elements, see e.g. Zhang et al. [4]. Therefore, a CFD prediction is dependent on many parameters such as the selected turbulence model, the software scheme, the grid number and grid distribution, the selected boundary conditions etc.

A way to select the right CFD procedure is to test the turbulence model and all other elements in geometry with a measured air distribution, which has some similarities to the room geometry for which we want to solve the flow. In this paper, we will make measurements in a geometry, which has been used earlier in two different workshops, namely in a workshop on the ISHVAC-COBEE conference in July 2015, see Peng et al. [5] and in a workshop on the Indoor Air Conference 2016, see van Hooff et al. [6]. It is a simple supply air flow scenario in building ventilation, similar to the backward-facing step flow. The turbulence models did very strongly influence the results of the work. Both workshops were designed as blind tests in which the measurements were unknown for the

participants so it was not possible to decide the quality level of the different predictions. The aim of this paper is, therefore to make measurements (a benchmark tests) in the above-mentioned geometry.

2. Turbulence models for room air distribution

The flow in a room with e.g. mixing ventilation is a combination of many different types of flow and flow elements.

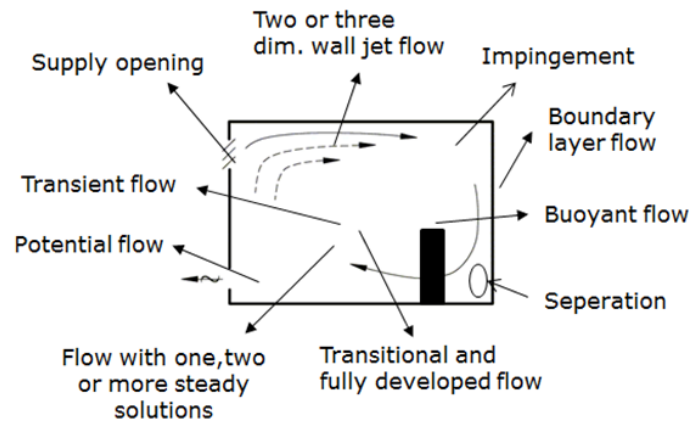


Figure 1. Examples of different types of flow in a room with mixing ventilation.

Some of the flow or flow elements in figure 1 can be solved separately by CFD. Different turbulence models are in fact optimized so as to solve the single flow elements, and it is therefore not obvious which turbulence model should be used in the case of a combined flow like the one in figure 1. Table 1 shows the turbulence models optimal for some of the flow elements.

Table 1. Flow elements and turbulence models

Flow Element	Supply opening [7]	Two or three dim. wall jet flow [4], [7], [8], [9], [10]	Buoyant flow [4]	Transitional and fully developed recirculating flow [4], [7], [8]
Turbulence Models	<i>LRN</i>	<i>k-ε, k-ω, BSL, v²-f, RSM</i>	<i>SST</i>	<i>k-ε family, LRN, v²-f</i>

The air movement in the **supply opening** can be a flow with a low turbulence level due to design details as contraction etc. although it enters into a room with a high turbulence level, [7]. The low Reynolds number models (*LRN*) are an option for the direct study of the flow in the diffuser. The *k-ε* family, *k-ω* and *BSL* models work well for **two-dimensional wall jet flow**, [7] and [8]. For **three-dimensional flow** in a wall jet, there is a difference in growth rates parallel to ceiling and perpendicular to ceiling. This effect is handled by the Reynolds stress model (*RSM*) and partly by a *v²-f* model, [9], [10]. The effect is especially important in elongated rooms (and tunnels) but not so important in normal short rooms, [9]. The *SST k-ω* worked well for strong **buoyant flow** in, for example, smoke management and rooms with thermal loads, [4]. Finally, the *k-ε* model and especially the *RNG k-ε* and the *v²-f* models have the best overall performance compared to other models in **fully developed recirculating flow** [4]. Predictions with standard *k-ε*, realizable *k-ε* and *RNG k-ε* model in a livestock building room with a complicated geometry including slatted floor show that all three models in this situation produced acceptably, but slightly different solutions at the isothermal flow, Rong et al. [11]. **In transitional flow**, the low Reynolds number *k-ε* model (*LRN*) is a possibility, but

the workshops at the ISHVAC-COBEE conference, [5] and the workshop at the Indoor air Conference 2016, [6] show that it is a difficult situation to handle with CFD predictions.

It is obviously a difficult situation to decide a single turbulence model for a general solution of the flow in a room like the one in figure 1. A possible procedure therefore is to test the different models in geometry similar to the room. The ISHVAC-COBEE workshop geometry is an elongated room with a ventilation opening in one end wall (backward facing step flow), and the flow in this model is addressed the following.

3. The backward-facing step flow – measurements

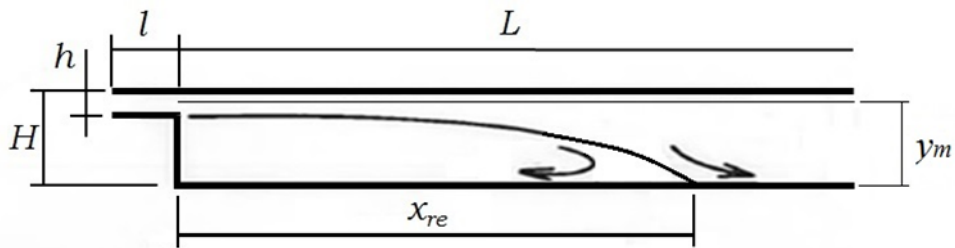


Figure 2. ISHVAC-COBEE model

Figure 2 shows the model of the backward-facing step flow. The model has the following dimensions: $h/H = 1/5 = 0.2$, $l/H = 4$, width $W = 2H$. Predictions are carried out in isothermal conditions with the Reynolds numbers, $0 < Re \leq 10,000$. The Re number is based on the inlet velocity and slot dimension. The length x_{re} is from the end wall to the location where the reattached flow is separated into a flow back to entrainment into the wall jet and a forward flow towards the exit (i.e. reattachment point). The length x_{re} is referred to as the penetration length of the supply jet, and it was selected as one of the parameters in the ISHVAC-COBEE workshop.

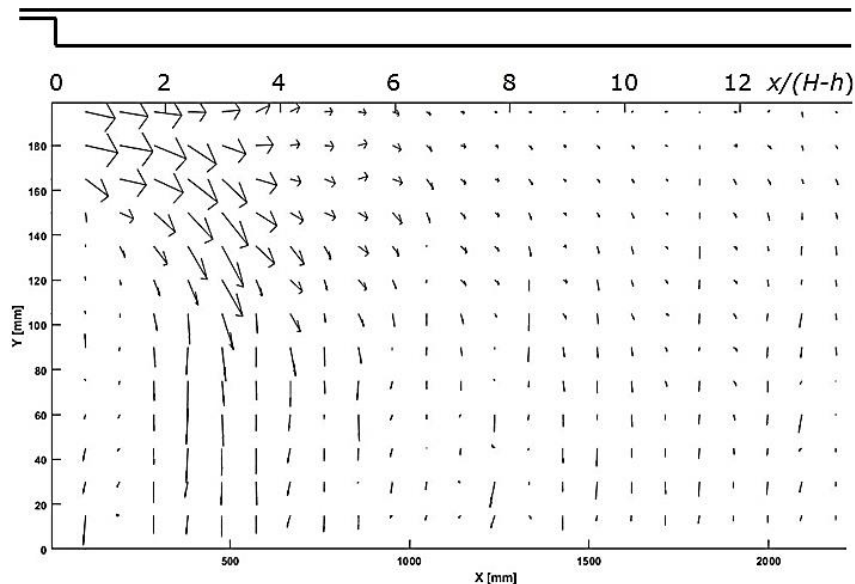


Figure 3. PIV measurements of the velocity distribution in the centre plane of the flow. $Re = 4000$.

A small scaled model made by acrylic is used in the measurement, with $h=0.04$ m and $L=3$ m, and the other dimensions are based on geometrical similarity as Figure 2. In order to validate isothermal condition assumption, six thermocouples are used to measure temperatures at model inlet, exhaust, surfaces and surrounding air. The velocity distribution in the model is measured by Particle Image

Velocimetry (PIV). The 2D-PIV system consists of a double cavity Nd:YAG laser with a wavelength of 532 nm, and a CCD camera with a resolution of 2048*2048 pixels.

Figure 3 is an example of the velocity distribution in the centre plane of the flow with Re number of 4000 (the y-axis is extended compared to the x-axis). The measurements do not give clear indication on the separation flow at the floor region and it is very difficult to locate the distance x_{re} in the model. It is more efficient to work with the measurements in the high velocity area of the flow. Therefore, we select the velocity distribution along a horizontal line in the height y_m as datasets for comparison with CFD predictions when the measurements are used as a benchmark, see figures 2 and 4.

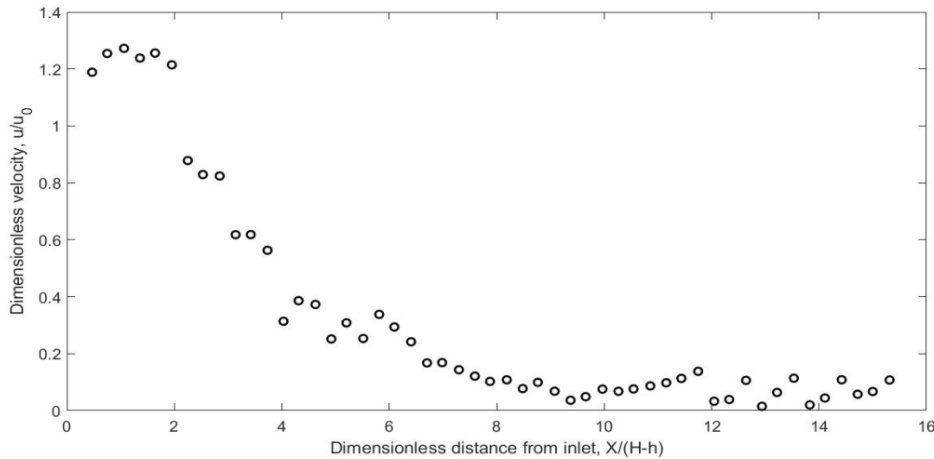


Figure 4. Velocity distribution in the height of $y_m/(H-h) = 1.19$. $Re = 4000$.

Measurements are made for $y_m/(H-h)$ equal to 0.34, 0.81 and 1.19 and for the Reynolds numbers $Re = 500, 1000, 4000,$ and $10,000$.

4. The backward-facing step flow, CFD predictions and comparison with measurements

Four different sets of CFD predictions are made for the backward-facing step flow where only the turbulence model is changed between the *RNG* $k-\epsilon$ model, the realisable $k-\epsilon$ model, the *BSL* $k-\omega$ model and the *SST* $k-\omega$ model. Other setup as mesh, boundary conditions and solving algorithms are unchanged. All the turbulence models utilized the near wall model approach, where the $k-\omega$ models are sufficient by themselves toward the edges and walls, while $k-\epsilon$ models needs modification near the wall. The Enhanced Wall Treatment is used since the y^+ -value is below 5 near the floor, Predictions are made in both a two-dimensional and a three-dimensional model. There are differences in the flow, so the conclusion is that the flow is three-dimensional.

Figure 5 and figure 6 show that it could be relevant to change turbulence model according to the supply velocity. The $k-\omega$ family seems to be an option for low turbulent flow ($Re = 500$) while the $k-\epsilon$ family looks as the best option for fully developed turbulent flow ($Re = 4,000$).

Several turbulence models can be relevant according to the different flow elements present in a room (see figure 1), and now it is also seen that the flow rate to the room can have an influence on the selection of the turbulence model.

The ISHVAC-COBEE workshop [5] and the Indoor Air 2016 workshop [6] show that CFD prediction is dependent on more parameters than the selected turbulence model. The software scheme, the order of accuracy, the grid number and grid distribution, the selected boundary conditions, the experience of the user, etc. and all the combinations are all parameters that can generate spreading of the results. We can illustrate this problem by comparing predictions from the ISHVAC-COBEE workshop with the predictions in this paper and earlier predictions at AAU.

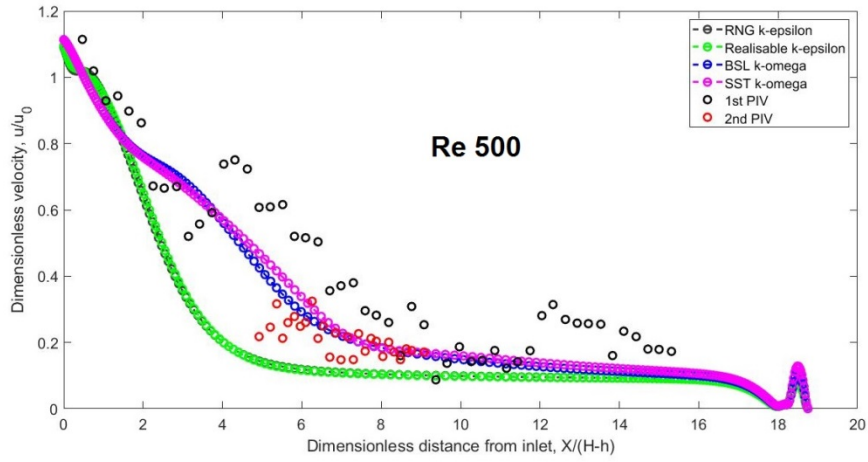


Figure 5. Comparison between measurements and predictions in the height $y_m/(H-h) = 1.19$. 3D flow and Reynolds number equal to 500.

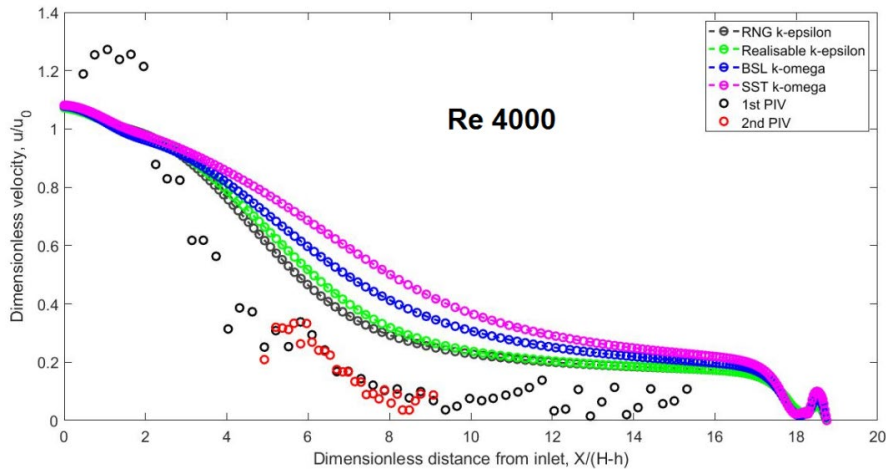


Figure 6. Comparison between measurements and predictions in the height $y_m/(H-h) = 1.19$. 3D flow and Reynolds number equal to 4000.

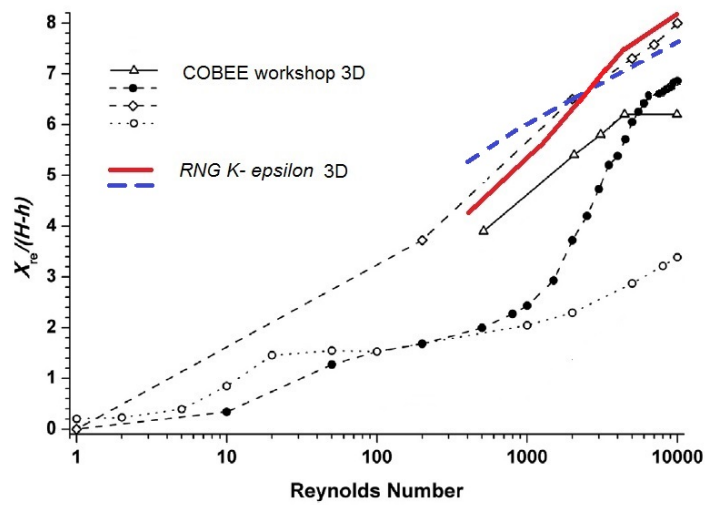


Figure 7. CFD predictions of the 3 D flow in the backward facing step model. All predictions are made with the *RNG k-ε* model. The present prediction is illustrated by a thick (red) curve and an earlier AAU prediction is shown by a dotted thick (blue) curve, [12].

All the predictions in figure 7 are made by the *RNG k-ε* turbulence model in a three-dimensional flow. They do not arrive at the same solution and they are influenced by some or all the different parameters mentioned above.

5. Conclusions

A benchmark is developed by making PIV measurements on the ISHVAC-COBEE model.

It is discussed that different turbulence models can solve the local flow elements in room air distribution optimally. It is therefore not so obvious which turbulence model should be used in the case of the combined flow in a room, but a number of promising models are introduced.

Results from benchmark test indicate that the *k-ω* family seems to be an option for low turbulent flow while the *k-ε* family looks as the best option for fully developed turbulent flow in the ISHVAC-COBEE model.

6. References

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